Chapter 5 Control volume approach and continuity equation

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Significant learning outcomes

Conceptual Knowledge

- Explain the key difference between the Lagrangian and Eulerian descriptions of a flow field.
- > Explain the meaning of volume flow rate and mass flow rate.
- > Explain what is meant by a system, control volume and control surface.
- State the purpose of the Reynolds transport theorem.
- Outline the steps in the derivation of the continuity equation.

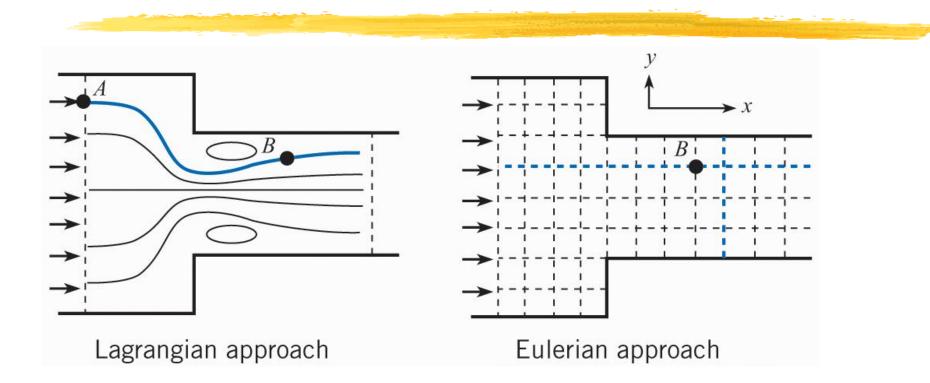
Procedural Knowledge

- Calculate the volume flow rate (discharge) and the mass flow rate.
- > Apply the continuity equation to draining tanks and reservoirs.
- > Apply continuity equation to velocity changes in variable-area ducts.

Applications (typical)

- > For flow through a Venturimeter, relate pressure, velocity, and flow rate.
- For a tank or reservoir, estimate draining time.
- For a small leak in a pressurized chamber, estimate depressurization time.

5.1 Lagrangian and Eulerian approach



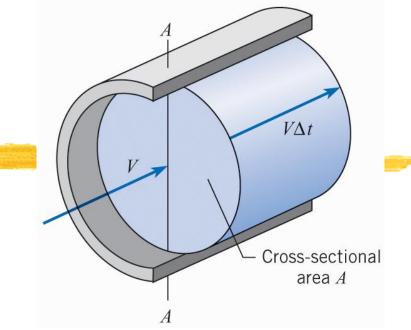
5.1 Rate of flow

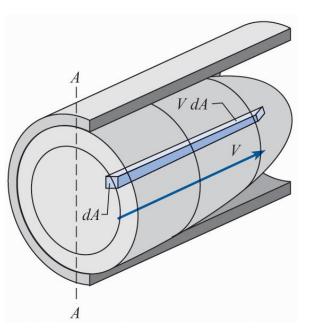
Discharge (volume flow rate):

Volume of fluid passing through an area per unit time.

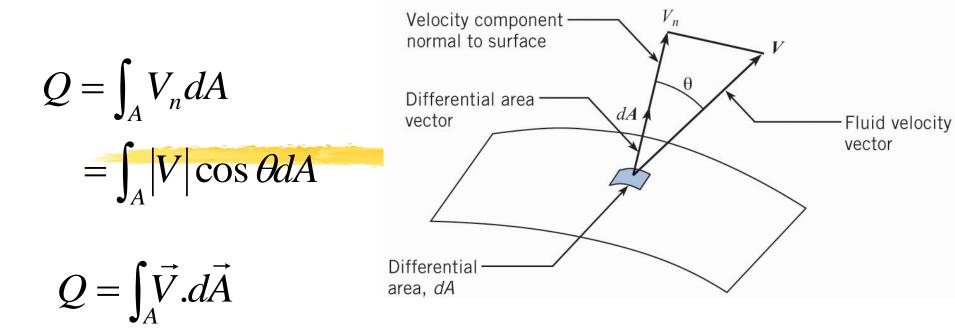
$$Q = \lim_{\Delta t \to 0} \frac{\Delta \Psi}{\Delta t} = VA$$

$$Q = \int_{A} V dA$$
$$\overline{V} = \frac{Q}{A}$$





CIVL 4046 Fluid Mechanics



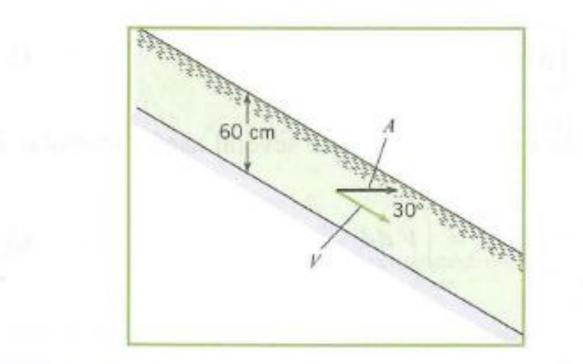
Mass flow rate: Mass of fluid passing through an area per unit time.

$$\dot{m} = \lim_{\Delta t \to 0} \frac{\Delta m}{\Delta t} = \rho \lim_{\Delta t \to 0} \frac{\Delta \Psi}{\Delta t} = \rho Q = \rho \overline{V}A$$
$$\dot{m} = \int_{A} \rho \overline{V} \cdot d\overline{A}$$

EXAMPLE 5.2 FLOW IN SLOPING CHANNEL

Water flows in a channel that has a slope of 30° . If the velocity is assumed to be constant, 12 m/s, and if a depth of 60 cm is measured along a vertical line, what is the discharge per meter of width of the channel?

Sketch:



Problem Definition

Situation: Channel slope of 30°. Velocity is 12 m/s and vertical depth is 60 cm.

Find: Discharge per meter width (m²/s). Assumptions: Velocity is uniformly distributed across channel.

Plan

Use Eq. (5.7) with area based on 1 meter width.

Solution

$$Q = V \cdot A = V \cos 30 \times A$$
$$= 12 \text{ m/s} \times \cos 30^{\circ} \times 0.6 \text{ m}$$
$$= 6.24 \text{ m}^3/\text{s per meter}$$

Review

The discharge per unit width is usually designated as q.

EXAMPLE 5.3 DISCHARGE IN CHANNEL WITH NON-UNIFORM VELOCITY DISTRIBUTION

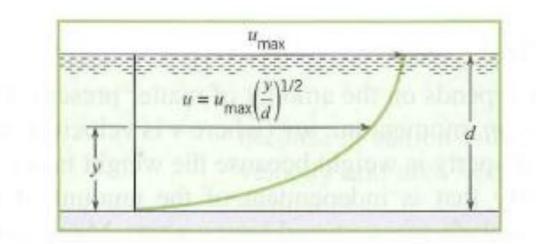
The water velocity in the channel shown in the accompanying figure has a distribution across the vertical section equal to $u/u_{max} = (y/d)^{1/2}$. What is the discharge in the channel if the water is 2 m deep (d = 2 m), the channel is 5 m wide, and the maximum velocity is 3 m/s?

Problem Definition

Situation: Water flows in a 2 m by 5 m channel with a given velocity distribution.

Find: Discharge (in m³/s).

Sketch:



Solution

Discharge equation

$$Q = \int_0^d u \, dA$$

Channel is 5 m wide, so differential area is dA = 5 dy. Using given velocity distribution,

$$Q = \int_0^2 u_{\max} (y/d)^{1/2} 5 \, dy$$

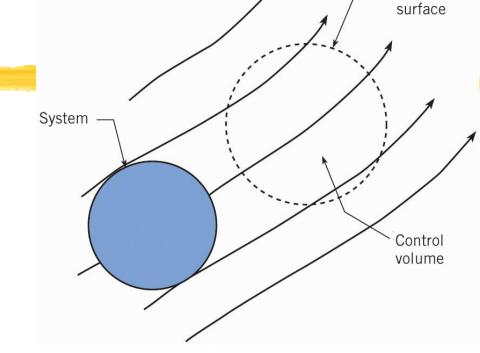
= $\frac{5u_{\max}}{d^{1/2}} \int_0^2 y^{1/2} \, dy$
= $\frac{5u_{\max}}{d^{1/2}} \frac{2}{3} y^{3/2} \Big|_0^2$
= $\frac{5 \times 3}{2^{1/2}} \times \frac{2}{3} \times 2^{3/2} = 20 \text{ m}^3/\text{s}$

5.2 Control volume approach

System and control volume

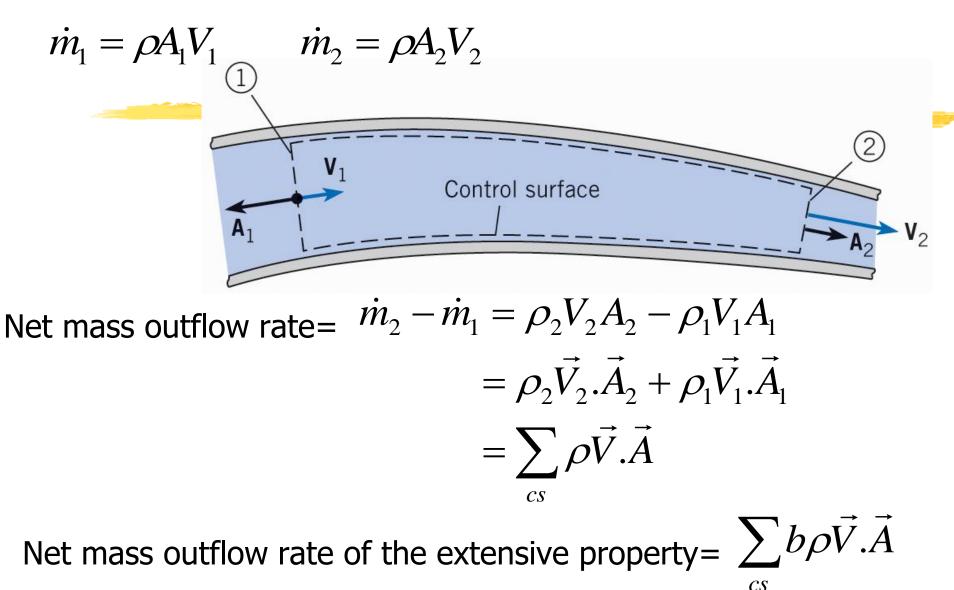
- Intensive Property: The property of a fluid that does not depend on the mass.
- Extensive Property: The property of a fluid that depends on the mass.

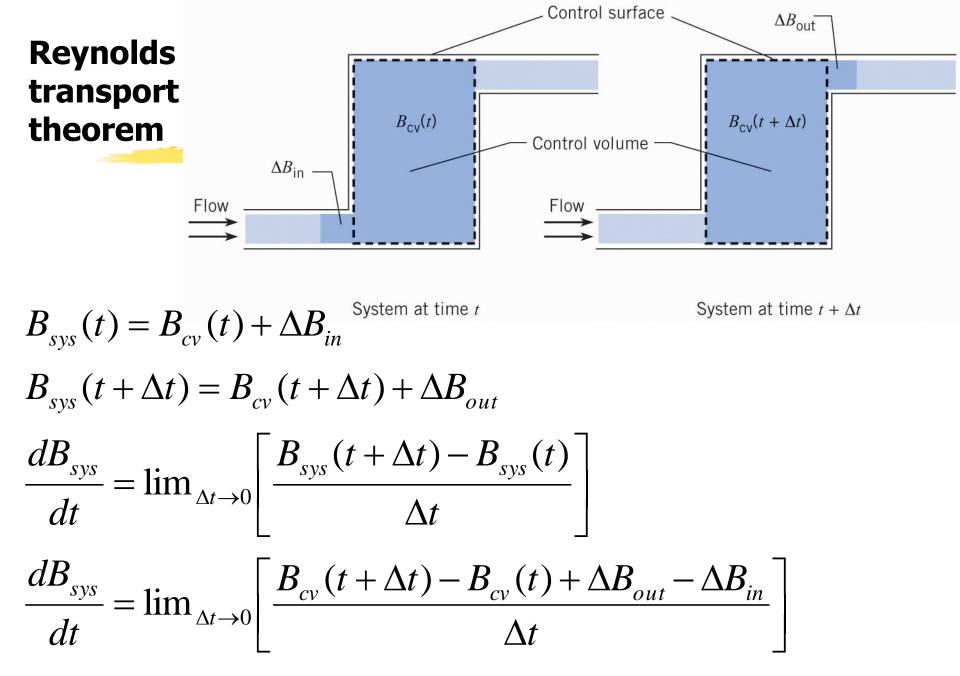
$$B_{cv} = \int_{cv} b\rho dV$$



Control

Property transport across the control surface





CIVL 4046 Fluid Mechanics

$$\frac{dB_{sys}}{dt} = \frac{dB_{cv}}{dt} + \dot{B}_{net}$$

$$\frac{dB_{sys}}{dt} = \frac{d}{dt} \int_{cv} b\rho dV + \int_{cs} b\rho \vec{V} \cdot d\vec{A}$$
Eulerian
$$5.3 \text{ Continuity equation}$$

$$B = m, \quad b = 1$$

$$\frac{dm_{sys}}{dt} = \frac{d}{dt} \int_{cv} \rho dV + \int_{cs} \rho \vec{V} \cdot d\vec{A}$$

$$\frac{dm_{sys}}{dt} = 0 \quad (\text{law of conservation of mass})$$

$$\frac{d}{dt} \int_{cv} \rho dV + \int_{cs} \rho \vec{V} \cdot d\vec{A} = 0$$

$$CVL 4046 \text{ Fluid Mechanics} \qquad 13$$

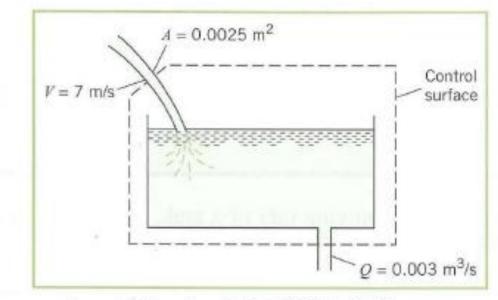
EXAMPLE 5.4 MASS ACCUMULATION IN A TANK

A jet of water discharges into an open tank, and water leaves the tank through an orifice in the bottom at a rate of 0.003 m^3/s . If the cross-sectional area of the jet is 0.0025 m² where the velocity of water is 7 m/s, at what rate is water accumulating in (or evacuating from) the tank?

Problem Definition

Situation: Jet of water (7 m/s at 0.0025 m²) entering tank and water leaving at 0.003 m³/s through orifice.

Find: Rate of accumulation (or evacuation) in tank (kg/s). Sketch:



Assumptions: Water density is 1000 kg/m³.

Solution

1. Continuity equation

$$\frac{d}{dt}m_{\rm ev} + \sum_{\rm es} \dot{m}_o - \sum_{\rm es} \dot{m}_j = 0$$

Because there is only one inlet and outlet, the equation reduces to

$$\frac{d}{dt}m_{\rm cv} = \dot{m}_i - \dot{m}_o$$

2. Term-by-term analysis

The inlet mass flow rate is calculated using Eq. (5.5)

$$\dot{m}_i = \rho V A$$

= 1000 kg/m³ × 7 m/s × 0.0025 m²

= 17.5 kg/s

Outlet flow rate is

$$\dot{m}_o = \rho Q = 1000 \text{ kg/m}^3 \times 0.003 \text{ m}^3/\text{s} = 3 \text{ kg/s}$$

3. Accumulation rate:

$$\frac{lm_{\rm cv}}{dt} = 17.5 \text{ kg/s} - 3 \text{ kg/s}$$
$$= 14.5 \text{ kg/s}$$

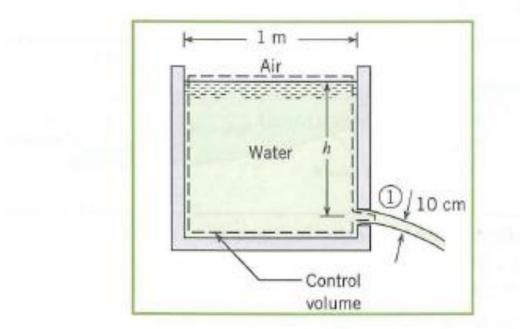
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EXAMPLE 5.6 WATER LEVEL DROP RATE IN DRAINING TANK

A 10 cm jet of water issues from a 1 m diameter tank. Assume that the velocity in the jet is $\sqrt{2gh}$ m/s where h is the elevation of the water surface above the outlet jet. How long will it take for the water surface in the tank to drop from $h_0 = 2$ m to $h_f = 0.50$ m?

Problem Definition

Situation: Water draining by a 10 cm jet from 1 m diameter tank. Find: Time (in seconds) to drain from depth of 2 m to 0.5 m. Sketch:



Solution

1. Continuity equation

$$\frac{d}{dt}m_{\rm cv} + \sum_{\rm cs} \dot{m}_o - \sum_{\rm cs} \dot{m}_i = 0$$

2. Term-by-term analysis

Accumulation rate term

$$\frac{dm_{\rm ev}}{dt} = \rho A_T \frac{dh}{dt}$$
$$\frac{dm_{\rm ev}}{dt} = \rho A_T \frac{dh}{dt}$$

where A_T is cross-sectional area of tank.

Inlet mass flow rate with no inflow is

$$\sum_{\rm cs} \dot{m}_i = 0$$

Outlet mass flow rate

$$\sum_{\rm cs} \dot{m}_o = \rho A_1 V_1 = \rho \sqrt{2gh} A_1$$

Substitution of terms in continuity equation:

$$-\rho V_1 A_1 = \frac{d(\rho A_T h)}{dt}$$
$$-\sqrt{2gh}A_1 = A_T \frac{dh}{dt}$$

- 3. Equation for elapsed time:
 - Separating variables

$$dt = \frac{-A_T}{\sqrt{2g}A_1} \frac{dh}{\sqrt{h}} \quad \text{or} \quad dt = \frac{-A_T}{\sqrt{2g}A_1} h^{-1/2} dh$$

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Integrating

$$t = \frac{-2A_T}{\sqrt{2g}A_1}h^{1/2} + C$$

Substituting in initial condition, h(0) = h₀, and final condition, h(t) = h_f, and solving for time

$$t = \frac{2A_T}{\sqrt{2g}A_1}(h_0^{1/2} - h_f^{1/2})$$

- 4. Time calculation:
 - Evaluating tank and outlet areas

$$A_1 = \frac{\pi}{4} (0.10 \text{ m})^2 = 0.01 \left(\frac{\pi}{4}\right) \text{m}^2$$
$$A_T = \frac{\pi}{4} D^2 = \frac{\pi}{4} \times (1 \text{ m})^2 = \frac{\pi}{4} \text{ m}^2$$

Elapsed time

$$t = \frac{2(\pi/4) \text{ m}^2}{\sqrt{2 \times 9.81 \text{ m/s}^2}(\pi/4 \times 0.01 \text{ m}^2)} (\sqrt{2 \text{ m}} - \sqrt{0.5 \text{ m}})$$

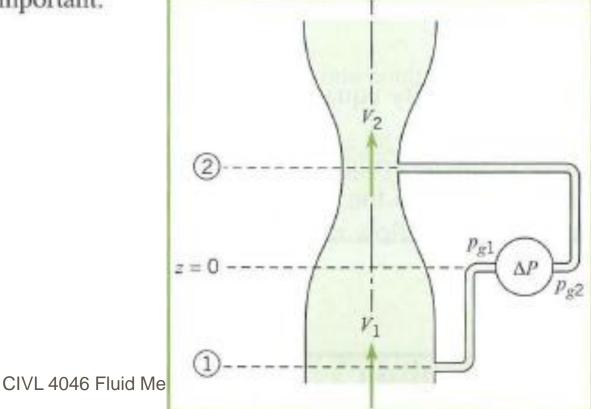
= 31.9 s

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Continuity equation for flow in a pipe $\frac{d}{dt} \int_{cv} \rho dV + \int_{cs} \rho \vec{V} \cdot d\vec{A} = 0$ $\frac{d}{dt} \int_{cv} \rho d\Psi = 0 \quad \text{(steady flow)}$ Control surface 2 $\int_{CS} \rho \vec{V} \cdot d\vec{A} = 0$ $\sum \dot{m}_{out} = \sum \dot{m}_{in}$

EXAMPLE 5.9 WATER FLOW THROUGH A VENTURIMETER .

Water with a density of 1000 kg/m³ flows through a vertical venturimeter as shown. A pressure gage is connected across two taps in the pipe (station 1) and the throat (station 2). The area ratio $A_{\text{throat}}/A_{\text{pipe}}$ is 0.5. The velocity in the pipe is 10 m/s. Find the pressure difference recorded by the pressure gage. Assume the flow has a uniform velocity distribution and that viscous effects are not important.



Solution

1. The Bernoulli equation

$$p_1 + \gamma z_1 + \rho \frac{V_1^2}{2} = p_2 + \gamma z_2 + \rho \frac{V_2^2}{2}$$

Rewrite the equation in terms of piezometric pressure.

$$p_{z_1} - p_{z_2} = \frac{\rho}{2} (V_2^2 - V_1^2)$$
$$= \frac{\rho V_1^2}{2} \left(\frac{V_2^2}{V_1^2} - 1 \right)$$

2. Continuity equation $V_2/V_1 = A_1/A_2$

$$p_{z_1} - p_{z_2} = \frac{\rho V_1^2}{2} \left(\frac{A_1^2}{A_2^2} - 1 \right)$$
$$= \frac{1000 \text{ kg/m}^3}{2} \times (10 \text{ m/s})^2 \times (2^2 - 1)$$
$$= 150 \text{ kPa}$$

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3. Gage is located at zero elevation. Apply hydrostatic equation through static fluid in gage line between gage attachment point where the pressure is p_{g_1} and station 1 where the gage line is tapped into the pipe,

$$p_{z_1} = p_{g_1}$$

Also
$$p_{z_2} = p_{g_2}$$
 so

$$\Delta p_{gage} = p_{g_1} - p_{g_2} = p_{z_1} - p_{z_2} = 150 \text{ kPa}$$